

A novel concept for treatment of the domestic sewage: Sequential batch biofilm reactor

Hiral Jariwala^{1*}, Dimpri Shah²

Department of Environmental Engineering, L. D. College of Engineering, Ahmedabad-380015, Gujarat, INDIA.

Email: jariwalahj@yahoo.com

Abstract

With the introduction of the stringent standard by pollution control board, it is our responsibility to treat the sewage to comply the standards of receiving streams. Nowadays a new trend is developed to adopt the combination of suspended and attached growth process for wastewater treatment. In SBR, four processes fill, aeration, settling and decanting take place with certain retention time where microorganisms are present in suspended form. In MBBR, microorganism's growth take place on the PVC media in aeration tank and secondary settling take place in another tank with certain retention time. So the present study will show the feasibility of Sequential Bed Biofilm Reactor (SBBR) with combined suspended and attached growth system. Compared with an SBR and MBBR, SBBR has many advantages, such as more biomass and higher removal efficiency, less sludge and sludge conglomeration, greater volumetric loads and increased process stability toward shock loadings. The main advantage of SBBR compare to SBR and MBBR is higher nutrient removal efficiency in the context of nitrogen and phosphorus removal. The study will show COD, BOD and, TKN parameter with different detention time and organic loading.

Key Words: Sequential Batch Biofilm Reactor; Sequential Batch Reactor; Moving Bed Biofilm Reactor; Nutrient Removal; PVC media.

* Address for Correspondence:

Dr. Hiral Jariwala, Department of Environmental Engineering, L. D. College of Engineering, Ahmedabad-380015, Gujarat, INDIA.

Email: jariwalahj@yahoo.com

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INTRODUCTION

Wastewater treatment is becoming crucial day by day due to increasing the wastewater generation in city due population explosion. Growth of urbanization in India is at rapid rate. As per the WATER (PREVENTION AND CONTROL OF POLLUTION) ACT, 1974 "Sewage Effluent" means effluent from any sewerage system or sewage disposal works and includes sullage from open drains. In India, most of the cities have conventional sewage treatment plant (ASP based) and ASP based treatment plant's BOD removal efficiency is 60-70%, COD removal efficiency is 55-65% and Ammonical Nitrogen removal is 10-20 %*. Whereas modern

technologies like SBR and MBBR can overcome these challenges¹⁰. We are striving for the solutions where domestic sewage treatment can become more advance.

MATERIALS AND METHODS

Pilot scale reactor: The experiments were carried out in lab-scale reactor; the SBBR as illustrated in Fig. 1. Reactor is made up of 2mm thickness Mild Steel (MS) sheet. The design of SBBR is done with the basic principles of the SBR and MBBR. The capacity of reactor is 300 L/day. The reactor was operated as SBBR. SBBR was filled with the biomedica 25% of the working volume⁵. Compressed air was supplied via diffusers at the bottom of the SBBR reactor. Mixing was performed in separate anoxic provided in the system. This SBBR system is working with the pre-anoxic system because its required carbon source to convert nitrate into nitrogen gas for efficient removal of Total Nitrogen from the wastewater. The dissolved oxygen (DO) concentrations were maintained above 3mg/L in the SBBR. Experiments were conducted at room temperature. Minimum DO concentration was maintained 2-3mg/L throughout the pilot scale set up to maintain the biofilm under appropriate conditions¹². Activated sludge was obtained from a local municipal WWTP as a seeding material to

the reactor. Wastewater was fed and discharged by means of the Bernoulli's principle. The procedures of the reactor operation, such as feeding, aerating, settling and decanting, were controlled time to time by manually.

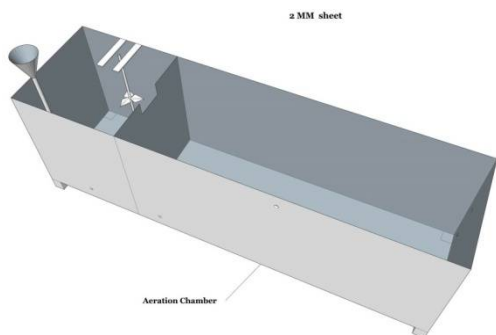


Figure 1: SBBR Reactor

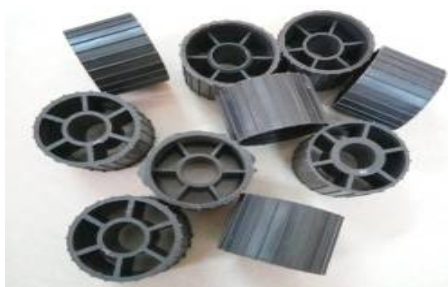


Figure 2: PVC media

There are two chambers in reactor: Anoxic and Aerobic. First wastewater passes through the anoxic chamber where incoming wastewater carbon reacts with the nitrate and that converts into nitrogen gas. PVC virgin plastic media is used with $400 \text{ m}^2/\text{m}^3$ surface area.

Experimental Procedure: In this study, Cycle is set for 6 hour. Filling (10 minute), Aeration (4 hour), Settling (1 hour and 30 minute), Decanting (5 minute), Recycle to Anoxic tank for reaction by manually (15 minute).

In the initial setup period reactor has worked 3 weeks for commissioning phase. Results were taken after the steady state condition is achieved.

Analytical Methods: All samples were analysed for COD, BOD_3 and Total Kjeldahl Nitrogen. The analytical methods were carried out as dictated by the APHA standard methods. In each experiment, the concentration of both attached and suspended biomass was measured as MLSS.

Pilot scale set up of SBBR



Figure 3: Pilot scale SBBR prototype

RESULTS AND DISCUSSION

Present study deals with the raw sewage with the preliminary treatment in grit chamber. Fig. 3 shows that effluent BOD profile in operation SBBR. Average influent COD concentration is $383 \pm 40 \text{ mg/L}$. The COD removal efficiency was $89 \pm 3 \%$.

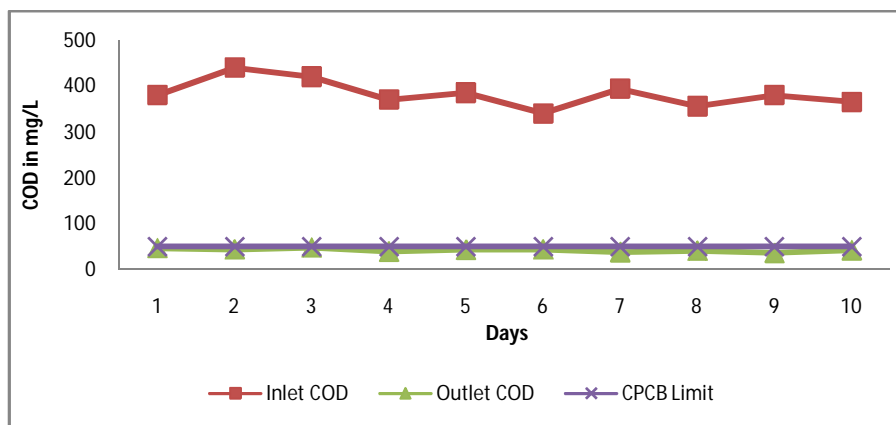


Figure 4: COD removal during SBBR operation

Figure 5 shows that effluent BOD profile in operation SBBR. The influent BOD concentration is 135 ± 15 mg/L and BOD removal efficiency was 92 ± 2 % achieved during the normal operation of SBBR.

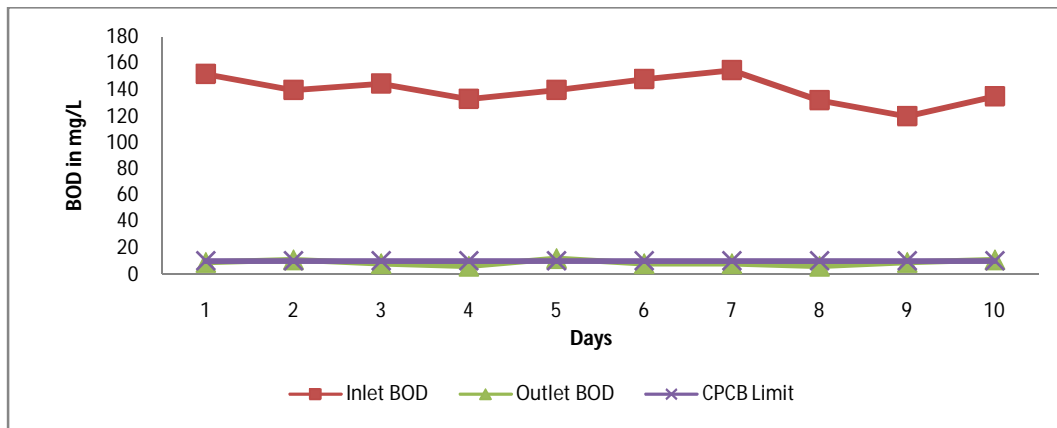


Figure 5: BOD removal during SBBR operation

Figure 6 shows that effluent TKN profile in operation SBBR. The influent TKN concentration is 25 ± 5 mg/L and TKN removal efficiency was 65 ± 10 % achieved during the SBBR operation.

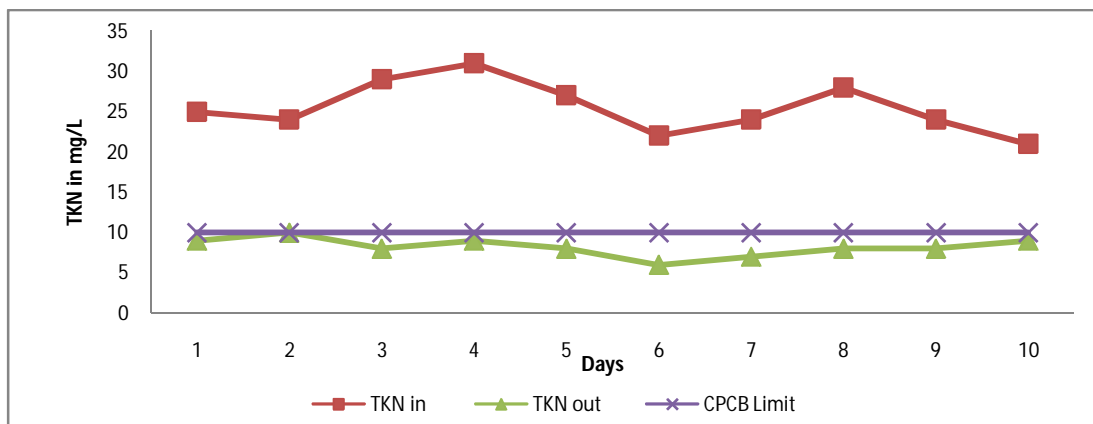


Figure 6: TKN removal during SBBR operation

Figure 7 shows that MLSS profile in operation SBBR. After 4 weeks of commissioning of the SBBR reactor MLSS concentration is achieved 2492.5 ± 200 mg/L.

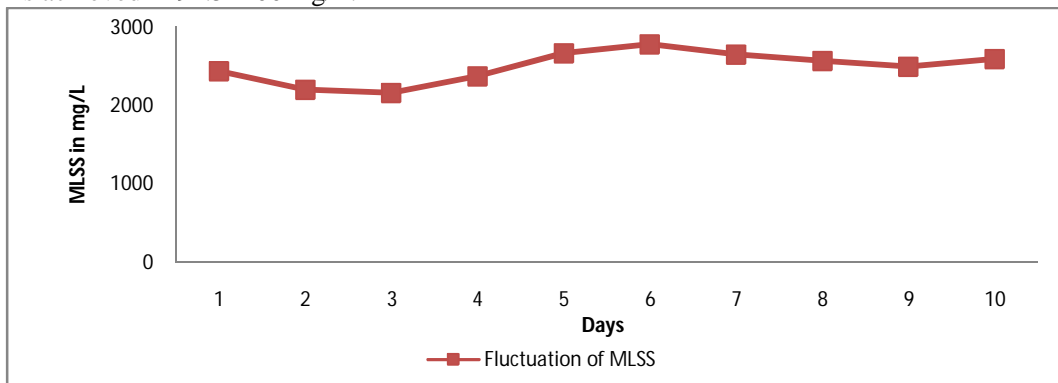


Figure 7: MLSS profile during the study period

CONCLUSION

The SBBR was designed to provide a compact and cost-effective treatment solution for wastewater compare to SBR and MBBR. The small scale 300 L/day SBBR prototype is working efficiently as the results showed in the paper. As the wastewater characteristics varied, recovery took more time to reach steady state conditions for the SBBR. The MLSS variation is occurred due to variation in influent characteristics. The results show that SBBR is working better compare to SBR and MBBR due to better process performance as COD, BOD, and TKN removal.

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